# Sulfated and persulfated TiO<sub>2</sub>/MCM-41 prepared by grafting method and their acid-catalytic activities for cyclization of pseudoionone

Dai-Shi Guo<sup>a</sup>, Zi-Feng Ma<sup>a,\*</sup>, Qi-Zhong Jiang<sup>a</sup>, Hai-Hong Xu<sup>a</sup>, Zheng-Fei Ma<sup>b</sup>, and Wei-Dong Ye<sup>c</sup>

<sup>a</sup>Department of Chemical Engineering, Shanghai Jiao Tong University, Shanghai 200240, P.R. China <sup>b</sup>College of Chemistry and Chemical Engineering, Nanjing University of Technology, Nanjing 210009, P.R. China <sup>c</sup>Xinchang Pharmaceutical Factory, Zhejiang Pharmaceutics Co. Ltd., Xinchang 312500, P.R. China

Received 2 November 2005; accepted 19 December 2005

Solid acid catalysts of  $SO_4^{2-}/TiO_2/MCM-41$  and  $S_2O_8^{2-}/TiO_2/MCM-41$  were prepared via grafting method and sulfate/persulfate promotion. The catalysts exhibited desirable activity and better selectivity for cyclization reaction of pseudoionone compared to traditional  $SO_4^{2-}/TiO_2$ . A combination of XRD,  $N_2$  adsorption—desorption and FTIR spectroscopy indicated that the catalysts possess well-ordered mesostructure, and the grafted  $TiO_2$  are in highly dispersed amorphous form rather than crystalline phase. For  $S_2O_8^{2-}/TiO_2/MCM-41$  higher S content and more Brønsted acid sites can be achieved by persulfation, which is favorable for the protons participated cyclization reaction. The similar Si-O-Ti-O-S=O structure of all acid sites on pore surface of the catalysts is attributed to the improvement of selectivity in comparison with  $SO_4^{2-}/TiO_2$ .

KEY WORDS: grafted TiO<sub>2</sub>; sulfate/persulfate promotion; MCM-41; cyclization of pseudoionone.

#### 1. Introduction

SO<sub>4</sub><sup>2</sup>/TiO<sub>2</sub> is a well-known catalyst for many acidcatalyzed reactions, such as isomerization [1], alkylation [2], esterification [3], acylation [4], nitration [5], condensation [6], and oligomerization [7]. However, the relatively small surface area and non-porous structure of  $SO_4^{2-}/TiO_2$  is unfavorable for its catalytic performance. In recent years, chemical grafting method has been applied to introduce highly dispersed TiO2 onto mesoporous silica to obtain materials with well-ordered mesostructure and large surface area [8-11]. The grafted TiO<sub>2</sub> in the resulting materials are mainly isolated tetrahedrally coordinated species and in amorphous form rather than anatase phase as conventional  $SO_4^{2-}/TiO_2$ . Though the Ti content is low, all the active Ti sites in the resulting materials are located on pore surface via Si-O-Ti bonds, thus structurally well defined and easily accessible. It has been shown that this kind of catalysts exhibited good activities for photocatalytic and epoxidation reactions [8–11]. However, there were no reports yet on sulfate treatment of TiO<sub>2</sub> grafted mesoporous silica for acid-catalysis purpose.

The isomeric ionones are of both academic and commercial interest, and have been widely used as fragrance, starting materials or building blocks in synthesis of medicine and many fine chemical products [12]. Ionones are usually produced via cyclization of pseudoionone catalyzed by concentrated liquid acids under rigorous conditions [13–16], and this process essentially

results in separation difficulties and environmental problems, to which an efficient solution is the employment of solid acid catalysts. Additionally, there were no reports on cyclization reactions catalyzed with  $SO_4^{2-}/TiO_2$  until now. These reasons drive us to develop a  $TiO_2$  modified catalyst with well-ordered mesostructure for the cyclization of bulky pseudoionone molecule.

In this work, MCM-41 was modified with  $TiO_2$  by grafting method, and promoted with  $H_2SO_4$  and  $(NH_4)_2S_2O_8$  aqueous solutions.  $TiO_2$  grafted MCM-41 without sulfation/persulfation and the traditional nanosized  $SO_4^{2-}/TiO_2$  were also prepared for comparison. The structural and acid properties of the catalysts were characterized with XRD,  $N_2$  adsorption–desorption, and FTIR spectroscopy, and their catalytic performances for cyclization of pseudoionone to ionones were examined. The obtained  $SO_4^{2-}/TiO_2/MCM$ -41 and  $S_2O_8^{2-}/TiO_2/MCM$ -41 exhibited desirable acid-catalytic activity and better selectivity for the cyclization reaction in comparison to  $SO_4^{2-}/TiO_2$ .

### 2. Experimental

# 2.1. Catalyst preparation

Pure siliceous MCM-41 was synthesized following the procedure proposed by Grün et al. [17]. The new solid acid catalysts of SO<sub>4</sub><sup>2</sup>/TiO<sub>2</sub>/MCM-41 and S<sub>2</sub>O<sub>8</sub><sup>2</sup>-/TiO<sub>2</sub>/MCM-41 were prepared through grafting reaction of Ti(OBu<sup>n</sup>)<sub>4</sub> with Si–OH on pore surface of MCM-41 and sulfate/persulfate promotion. Pre-calcined MCM-41 was stirred in mixed solution of excess Ti(OBu<sup>n</sup>)<sub>4</sub> (C.P.,

<sup>\*</sup>To whom correspondence should be addressed. E-mail: zfma@sjtu.edu.cn

Shanghai Chemical Reagent Co.) and dehydrated *n*-hexane at 70 °C to form surface Si–O–Ti–OBu groups, washed with anhydrous ethanol to remove residual Ti(OBu<sup>n</sup>)<sub>4</sub> thoroughly, and hydrolyzed in deionized water at room temperature to generate Si–O–Ti–OH on silica wall. The filtered and dried solid was impregnated with 0.5 M H<sub>2</sub>SO<sub>4</sub> and (NH<sub>4</sub>)<sub>2</sub>S<sub>2</sub>O<sub>8</sub> solution, respectively, followed by drying and calcination at 450 °C for 3 h to get SO<sub>4</sub><sup>2</sup>/TiO<sub>2</sub>/MCM-41 and S<sub>2</sub>O<sub>8</sub><sup>2</sup>/TiO<sub>2</sub>/MCM-41. TiO<sub>2</sub>/MCM-41 without sulfation was obtained by calcining the hydrolyzed solid directly.

Nanosized  $SO_4^{2-}/TiO_2$  was prepared through hydrolysis of TiCl<sub>4</sub>. Pre-cooled TiCl<sub>4</sub> (98%, Shanghai Meixing Chemical Co. Ltd.) was added dropwise into dilute HCl solution in ice-bath under vigorous stirring. After stabilization at 0–15 °C for 30 min, aqueous ammonia was added drop by drop at 70 °C under constant stirring until pH=9. The precipitate was treated with 0.5 M  $H_2SO_4$  solution and calcined at 450 °C to obtain  $SO_4^{2-}/TiO_2$ .

# 2.2. Catalyst characterization

The XRD patterns were collected by Shimadzu XRD-6000 diffractometer using Ni-filtered CuKα radiation operating at 40 kV and 30 mA. N<sub>2</sub> adsorption desorption isotherms were measured with Quantachrome NOVA 1000 at 77 K. Before measurement the samples were outgassed at 300 °C for 3 h. FTIR spectra were recorded with Nicolet Avartar 360 spectrophotometer. KBr pellets with 1.0 wt.% catalysts containing were used to collect vibration spectra of Si-O-Ti bonds, while self-supporting catalysts wafers were used to characterize the S = O vibration, as well as the presence of Brønsted and Lewis acid sites by pyridine adsorption. The wafers were evacuated at 400 °C for 3 h in an in situ cell under vacuum at  $6 \times 10^{-2}$  Pa before scanning. Ti content of the catalysts was analyzed with IRIS ADVANTAGE/1000 ICP-AES, and S content was determined with PE 2400II CHNS/O Analyzer.

# 2.3. Catalytic testing

The cyclization reaction of pseudoionone to ionones was carried out in a 100 mL flask reactor. The reactant (1.5 g of pseudoionone, >95%, Xinchang Pharmaceutical Factory) and the solvent (20 mL of cyclohexane) were introduced into the reactor. When the temperature was raised to 80 °C, 1.0 g of the catalysts was added under constant stirring. The products were analyzed on Angilent 6890N gas chromatograph with FID detector.

#### 3. Results and discussion

XRD patterns of the catalysts are presented in figure 1. The three peaks at low diffraction angles in figure 1(a) show the long-range ordered hexagonal

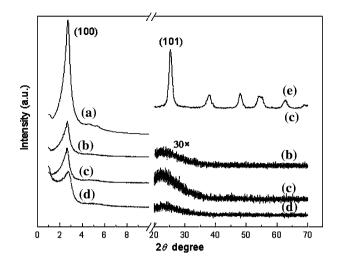


Figure 1. XRD patterns of (a) calcined MCM-41, (b) TiO<sub>2</sub>/MCM-41, (c)  $SO_4^2$  /TiO<sub>2</sub>/MCM-41, (d)  $S_2O_8^2$  /TiO<sub>2</sub>/MCM-41 and (e)  $SO_4^2$  /TiO<sub>2</sub>.

mesostructure of the pure siliceous MCM-41. For  $TiO_2/MCM$ -41,  $SO_4^{2-}/TiO_2/MCM$ -41 and  $S_2O_8^{2-}/TiO_2/MCM$ -41, the intensity of main reflection (100) peak decreased due to the  $TiO_2$  grafting, while the ordered mesoporous structure was generally kept. The intense peaks at  $2\theta$  range from 20 to 70 ° in figure 1(e) show the typical anatase phase of  $SO_4^{2-}/TiO_2$ , and the average  $TiO_2$  crystallite size was estimated to be 6.8 nm using Sherrer formula on the (101) peak. No peaks corresponding to crystalline  $TiO_2$  can be observed at the same  $2\theta$  range in figure 1(b), (c), and (d), indicating that the grafted  $TiO_2$  are in highly dispersed amorphous form without crystalline particles formed within or outside MCM-41 pores.

The BET data, Ti and S contents are listed in table 1. With  $TiO_2$  grafting and sulfation/persulfation, the BET surface area and total pore volume of  $TiO_2/MCM$ -41,  $SO_4^{2-}/TiO_2/MCM$ -41 and  $S_2O_8^{2-}/TiO_2/MCM$ -41 decreased in comparison with that of MCM-41, but they are still much higher than those of the nanosized  $SO_4^{2-}/TiO_2$ , and the slight shrinkage of their average pore size indicates the incorporation of  $TiO_2$  into MCM-41 mesopores.

Figure 2 shows the FTIR spectra of MCM-41 and its  $TiO_2$  modified samples. For  $TiO_2/MCM$ -41,  $SO_4^{2-}/TiO_2/MCM$ -41 and  $S_2O_8^{2-}/TiO_2/MCM$ -41, the band at ca. 966 cm<sup>-1</sup> corresponding to vibration of Si–O–Ti bonds [18] indicates that  $TiO_2$  have been successfully grafted onto MCM-41 wall. No peaks at 650 cm<sup>-1</sup> assignable to crystalline anatase were detected using FTIR. The characteristic S=O vibration bands of  $SO_4^{2-}/TiO_2$ ,  $SO_4^{2-}/TiO_2/MCM$ -41 and  $S_2O_8^{2-}/TiO_2/MCM$ -41 are presented in figure 3.  $SO_4^{2-}/TiO_2$  gave single S=O band at 1379 cm<sup>-1</sup>, while  $SO_4^{2-}/TiO_2/MCM$ -41 showed a band at 1409 cm<sup>-1</sup> and a shoulder at 1379 cm<sup>-1</sup>, corresponding to S=O induced from  $SO_4^{2-}/TiO_2/MCM$ -41 showed a band at S=O induced from  $SO_4^{2-}/TiO_2/MCM$ -41 showed a band at S=O induced from  $SO_4^{2-}/TiO_2/MCM$ -41 showed a band at S=O induced from  $SO_4^{2-}/TiO_2/MCM$ -41 showed a band at S=O induced from  $SO_4^{2-}/TiO_2/MCM$ -41 showed a band at S=O induced from  $SO_4^{2-}/TiO_2/MCM$ -41 showed a band at S=O induced from  $SO_4^{2-}/TiO_2/MCM$ -41 showed a band at S=O induced from  $SO_4^{2-}/TiO_2/MCM$ -41 showed a band at S=O induced from  $SO_4^{2-}/TiO_2/MCM$ -41 showed a band at S=O induced from  $SO_4^{2-}/TiO_2/MCM$ -41 showed a band at S=O induced from  $SO_4^{2-}/TiO_2/MCM$ -41 showed a band at S=O induced from  $SO_4^{2-}/TiO_2/MCM$ -41 showed a band at S=O induced from  $SO_4^{2-}/TiO_2/MCM$ -41 showed a band at S=O induced from  $SO_4^{2-}/TiO_2/MCM$ -41 showed a band at S=O induced from  $SO_4^{2-}/TiO_2/MCM$ -41 showed a band at S=O induced from  $SO_4^{2-}/TiO_2/MCM$ -41 showed a band at S=O induced from  $SO_4^{2-}/TiO_2/MCM$ -41 showed a band at S=O induced from  $SO_4^{2-}/TiO$ -41 showed a band at S=O-4 induced from  $SO_4^{2-}/TiO$ -41 showed a band at S=O-4 induced from  $SO_4^{2-}/TiO$ -41 showed a band at S=O-4 induced from  $SO_4^{2-}/TiO$ -4 induced from  $SO_4^{2-}/TiO$ -4 induced from  $SO_4^{2-}/TiO$ -4 induced from  $SO_4^{2-}/TiO$ -4 induced from

Samples	BET surface area (m <sup>2</sup> /g)	Pore volume (mL/g)	Average pore size (nm)	Ti content (wt.%)	S content (wt.%)
MCM-41	1226	0.74	2.41	_	
TiO <sub>2</sub> /MCM-41	816	0.47	2.31	4.28	_
$SO_4^{2-}/TiO_2/MCM-41$	823	0.49	2.38	4.24	0.87
$S_2O_8^{2-}/TiO_2/MCM-41$	691	0.39	2.26	4.14	3.18
$SO_4^{2-}/TiO_2$	167	0.20	4.71	_	4.01

Table 1
Physicochemical properties of the catalysts

 $SiO_2$  and  $SO_4^{2-}/TiO_2$ , respectively. For  $S_2O_8^{2-}/TiO_2/MCM$ -41, the additional band at 1398 cm<sup>-1</sup> can be assigned to  $S_2O_7^{2-}$  specie on  $TiO_2$  surface according to earlier report [19], and the band at 1379 cm<sup>-1</sup> results from decomposition of  $S_2O_8^{2-}$  into  $SO_4^{2-}$  during calcination. According to table 1,  $S_2O_8^{2-}/TiO_2/MCM$ -41 possesses a much higher S content than  $SO_4^{2-}/TiO_2/MCM$ -41, which indicates that  $S_2O_8^{2-}$  can be chelated more efficiently on the grafted  $TiO_2$  at a low surface Ti concentration (ca. 0.75 nm<sup>-2</sup> average by ICP and BET results in table 1) than  $SO_4^{2-}$ , because of its favorably larger kinetic diameter compared to  $SO_4^{2-}$  (0.31 nm<sup>2</sup>) [20].

The pyridine adsorption *in situ* FTIR spectra are present in figure 4. It can be found that  $SO_4^{2-}/TiO_2$ ,  $SO_4^{2-}/TiO_2/MCM$ -41 and  $S_2O_8^{2-}/TiO_2/MCM$ -41 contain both Brønsted (at  $1540~\rm cm^{-1}$ ) and Lewis (at  $1445~\rm cm^{-1}$ ) acid sites, while only Lewis acidity can be observed for  $TiO_2/MCM$ -41. It is obvious that the peak area at  $1540~\rm cm^{-1}$  was enlarged with the increase of S content list in table 1. For  $SO_4^{2-}/TiO_2$  and  $S_2O_8^{2-}/TiO_2/MCM$ -41 the Brønsted acidity was predominant, but  $SO_4^{2-}/TiO_2/MCM$ -41 showed more Lewis acidity. This result is coincident with the previous report [20] that Brønsted acidity was improved at higher S content.

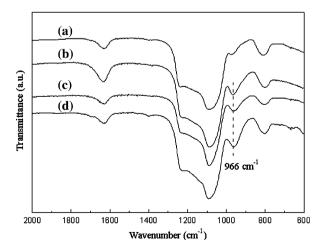


Figure 2. FTIR spectra of (a) calcined MCM-41, (b)  $TiO_2/MCM$ -41, (c)  $SO_4^2/TiO_2/MCM$ -41 and (d)  $S_2O_8^2/TiO_2/MCM$ -41.

It has been known that the major product of pseudoionone cyclization is the mixture of  $\alpha$ - and  $\beta$ -ionones (equation (1)), and the presence of numerous by-products was difficult to be avoided due to the complexity of the reaction [21]. It was also proposed that protons played a key role in the intra-molecule cyclization reaction [13]. Catalytic performance in this study was evaluated in terms of pseudoionone conversion X (equation (2)) and selectivity S of  $\alpha$ - and  $\beta$ -ionones (equation (3)), where  $a_f$  is the amount of pseudoionone in products, and  $a_i$  the amount of  $\alpha$ - and  $\beta$ -ionones in products.

pseudoionone 
$$\alpha$$
-ionone  $\beta$ -ionone (1)

$$X = 100 \times (a_f - a_p)/a_f \tag{2}$$

$$S = 100 \times a_i / (a_f - a_p) \tag{3}$$

The catalytic behavior of the solid acid catalysts is presented in figure 5 and table 2. It is shown in figure 5 that  $TiO_2/MCM$ -41 is almost not active, while activities of the other three catalysts were improved with the increase of S content and Brønsted acidity as illustrated in table 1 and figure 4, and  $S_2O_8^{2-}/TiO_2/MCM$ -41 possesses a catalytic performance comparable to nanosized  $SO_4^{2-}/TiO_2$ . This indicates that higher S content and more Brønsted acid sites are favorable for the proton participated cyclization reaction. Additionally, it can be found in table 2 that  $S_2O_8^{2-}/TiO_2/MCM$ -41 and  $SO_4^{2-}/TiO_2/MCM$ -41 have better selectivity of ionones compared to  $SO_4^{2-}/TiO_2$ .

It has been reported that acid activity can hardly be produced on  $SiO_2$  surface promoted with  $SO_4^{2-}$ , due to the relatively higher electronegativity and low coordination number of  $Si^{4+}$ , while the acidity of conventional  $SO_4^{2-}/TiO_2$  derives from the S=O induction on the edge or corner of anatase surface where the octahedral coordination is unsaturated [22]. For  $S_2O_8^{2-}/TiO_2/MCM-41$  and  $SO_4^{2-}/TiO_2/MCM-41$ , with the formation

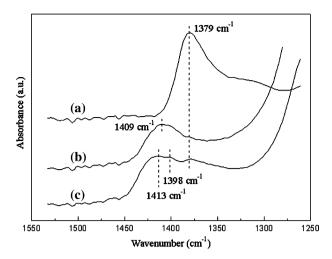


Figure 3. FTIR spectra of (a)  $SO_4^{2-}/TiO_2$ , (b)  $SO_4^{2-}/TiO_2/MCM-41$  and (c)  $S_2O_8^{2-}/TiO_2/MCM-41$ , after evacuation at 400 °C for 3 h.

of Si–O–Ti–O–S=O bonds on pore surface, both the electronegativity difference of Si from Ti as well as the S=O induction affect on Ti atoms to withdraw electron density to opposite directions, thus to produce desirable acid activity. Since  $S_2O_8^{2-}$  can be chelated onto the grafted TiO $_2$  species more efficiently than  $SO_4^{2-},\,S_2O_8^{2-}/TiO_2/MCM-41$  exhibited higher activity compared with  $SO_4^{2-}/TiO_2/MCM-41$ . On the other hand, all the acid sites on  $S_2O_8^{2-}/TiO_2/MCM-41$  and  $SO_4^{2-}/TiO_2/MCM-41$  can be speculated to possess similar structure of Si–O–Ti–O–S=O, which is favorable for improvement of the selectivity.

## 4. Conclusions

SO<sub>4</sub><sup>2</sup>/TiO<sub>2</sub>/MCM-41 and S<sub>2</sub>O<sub>8</sub><sup>2</sup>/TiO<sub>2</sub>/MCM-41 with well-ordered mesostructure were prepared through grafting reaction of Ti(OBu<sup>n</sup>)<sub>4</sub> with Si–OH on MCM-41

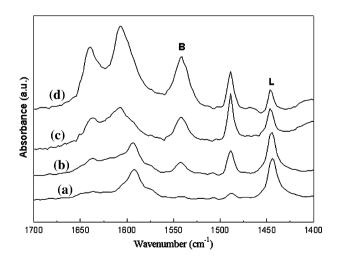


Figure 4. Pyridine adsorption FTIR spectra measured at 200 °C of (a) TiO<sub>2</sub>/MCM-41, (b) SO<sub>4</sub><sup>2</sup>/TiO<sub>2</sub>/MCM-41, (c) S<sub>2</sub>O<sub>8</sub><sup>2</sup>/TiO<sub>2</sub>/MCM-41 and (d) SO<sub>4</sub><sup>2</sup>/TiO<sub>2</sub>.

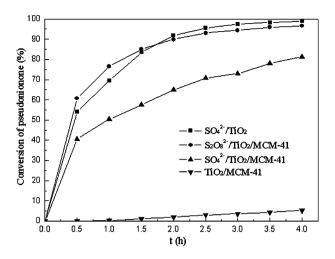


Figure 5. Activity of the catalysts for cyclization of pseudoionone at 80 °C.

Table 2 Selectivity of  $\alpha$ - and  $\beta$ -ionones of the catalysts

t (h)	Selectivity (%)				
	SO <sub>4</sub> <sup>2-</sup> /TiO <sub>2</sub>	SO <sub>4</sub> <sup>2-</sup> /TiO <sub>2</sub> /MCM-41	S <sub>2</sub> O <sub>8</sub> <sup>2-</sup> /TiO <sub>2</sub> /MCM-41		
1	21.92	17.24	25.64		
2	20.47	21.18	29.33		
3	18.90	23.70	29.25		
4	18.51	24.86	27.95		

wall and sulfate/persulfate treatment. Both of the catalysts exhibited desirable catalytic activity and better selectivity for cyclization reaction of pseudoionone compared to conventional  $SO_4^{2-}/TiO_2$ , although the grafted  $TiO_2$  are in amorphous form and at a low amount. The acid activity of  $SO_4^{2-}/TiO_2/MCM$ -41 and  $S_2O_8^{2-}/TiO_2/MCM$ -41 derives from the bilateral effect of electronegativity difference of Si from Ti as well as S=O induction on Ti atoms. Higher S content and more Brønsted acid sites are favorable for the protons needed cyclization reaction, and the acid sites with similar structure of Si-O-Ti-O-S=O are responsible for the better selectivity than  $SO_4^{2-}/TiO_2$ .

# Acknowledgments

The authors are grateful for the financial support of this work by the 863 Program of China under the approval of 2002AA323040, the National Science Foundation of China under the approval No. 20076026, 50236010, and 20476055, respectively.

# References

- A.K. Dalai, R. Sethuraman, S.P.R. Katikaneni and R.O. Idem, Ind. Eng. Chem. Res. 37 (1998) 3869.
- [2] S.K. Samantaray, T. Mishra and K.M. Parida, J. Mol. Catal. A: Chem. 156 (2000) 267.

- [3] G.Z. Lu, Appl. Catal. A: Gen. 133 (1995) 11.
- [4] Y.D. Xia, W.M. Hua and Z. Gao, Catal. Lett. 55 (1998) 101.
- [5] K.R. Sunajadevi and S. Sugunan, Catal. Commun. 9 (2005) 611.
- [6] C. Venkatesan and A.P. Singh, J. Mol. Catal. A: Chem. 181 (2002) 179.
- [7] A. Mantilla, F. Tzompantzi, G. Ferrat, A. Lopez-Ortega, E. Romero, E. Ortiz-Islas, R. Geomez and M. Torres, Chem. Commun. (2004) 1498.
- [8] T. Maschmeyer, F. Rey, G. Sankar and J.M. Thomas, Nature 378 (1995) 159.
- [9] S. Zheng, L. Gao, Q.H. Zhang and J.K. Guo, J. Mater. Chem. 10 (2000) 723.
- [10] M. Widenmeyer, S. Grasser, K. Köhler and R. Anwander, Micropor. Mesopor. Mater. 44–45 (2001) 327.
- [11] G. Galleja, R. van Grieken, R. García, J.A. Melero and J. Iglesias, J. Mol. Catal. A: Chem. 182–183 (2002) 215.

- [12] E. Brenna, C. Fuganti, S. Serra and P. Kraft, Eur. J. Org. Chem. (2002) 967.
- [13] E.E. Royals, Ind. Eng. Chem. 38 (1946) 546.
- [14] H. Otto, K. Hans and A. Lothar, US 4565894 (1986).
- [15] S. Kurt, E. Herwig and T. Helmut, US 5453546 (1995).
- [16] R. Udo, H. Ulrich and W. Dietmar, US 6288282 (2001).
- [17] M. Grün, I. Lauer and K.K. Unger, Adv. Mater. 9 (1997) 254.
- [18] X. Gao and I.E. Wachs, Catal. Today 51 (1999) 233.
- [19] Y.D. Xia, W.M. Hua and Z. Gao, Chem. Commun. (1999) 1899.
- [20] N. Katada, J. Endo, K. Notsu, N. Yasunobu, N. Naito and M. Niwa, J. Phys. Chem. B 104 (2000) 10321.
- [21] E.T. Theimer, Fragrance Chemistry: The Science of the Sense of Smell (Science Press, Beijing, 1989).
- [22] T. Yamaguchi, Appl. Catal. 61 (1990) 1.