# The effect of water and reductants on the release of nitrogen oxides stored on BaO/Al<sub>2</sub>O<sub>3</sub>

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The effect of water and reductants (CO and  $H_2$ ) on the decomposition of  $NO_x$  stored on  $BaO/Al_2O_3$  at 300 °C has been investigated. Water eliminates the initial rapid total uptake of  $NO_2$  but has little effect on the subsequent formation of nitrates that is accompanied by evolution of NO. Water hinders liberation of  $NO_2$  and NO during temperature-programmed decomposition of stored  $NO_x$ . Both CO and  $H_2$  lower the temperatures required for decomposition through reduction of  $NO_2$  to NO and  $N_2$  thus restricting  $NO_2$  readsorption. The rate of reduction is lower with  $H_2$  than with CO.

**KEY WORDS:** NO<sub>x</sub> storage catalysts; barium oxide; aluminum oxide; decomposition of stored nitrate; reduction of stored nitrate.

### 1. Introduction

Catalysts that operate via the sequential storage and reduction of nitrogen oxides are an effective technology for emission control of gasoline direct injection engines operating in lean-burn mode if sufficiently low sulfur fuel is available [1,2]. Platinum is used to oxidize NO during lean operation, the resulting  $NO_2$  being stored on a basic oxide such as that of barium [3]. A subsequent period of rich operation destabilizes the stored  $NO_x$  which is then reduced to nitrogen on the platinum and/ or the rhodium or palladium that is included to provide standard three-way catalysis during stoichiometric operation.

Work over the past few years has established many details of the chemistry involved in NO<sub>x</sub> storage catalysts with the storage process proving rather complex [4]. Infrared studies confirm that NO<sub>2</sub> is stored more strongly than NO with surface nitrite species seen first followed by nitrates [4,5], the latter also being detectable in bulk by X-ray diffraction (XRD) [4,6,7]. The conversion of NO<sub>2</sub> to NO<sub>3</sub> implies oxidation, with O<sub>2</sub> or NO<sub>2</sub> as the possible oxidants. In recent work using BaO/Al<sub>2</sub>O<sub>3</sub> we have shown that O<sub>2</sub> is not used even if it is present in large excess [8]. Instead some NO<sub>2</sub> is converted to NO with the overall uptake stoichiometry corresponding to approximately

$$BaO(s) + 3NO_2(g) \longrightarrow Ba(NO_3)_2(s) + NO(g)$$
 (1)

Evolution of NO is also apparent during NO<sub>2</sub> uptake when Pt is present [9] but NO<sub>2</sub>/NO equilibration on the metal is a possible complication in that case. Likewise, the presence of Pt may alter the NO<sub>2</sub>/NO distribution

during temperature-programmed decomposition of stored  $NO_x$ . With Pt/BaO/Al<sub>2</sub>O<sub>3</sub>, NO alone is seen in some studies [10] whereas BaO/Al<sub>2</sub>O<sub>3</sub> yields two peaks with NO<sub>2</sub> evolved at ~460 °C followed by NO above 500 °C [8]. Alumina stores NO<sub>2</sub> to a much lesser extent, with proportionately less evolution of NO, and it is released as a single peak of NO<sub>2</sub> at ~430 °C [8].

Under exhaust gas conditions Ba(OH)<sub>2</sub> and BaCO<sub>3</sub> are thermodynamically favored over BaO so NO<sub>x</sub> storage may take place with displacement of water or CO<sub>2</sub> rather than by simple nitrate formation. Some recent calculations indicate that conversion of bulk BaCO<sub>3</sub> to bulk Ba(NO<sub>3</sub>)<sub>2</sub> becomes unfavorable at elevated temperature (>150 °C [7] or 340 °C [8]) during lean operation, a possible implication being that storage occurs on a dispersed surface phase rather than as a bulk one. The presence of the former has been inferred from quantitative XRD studies showing that bulk BaCO<sub>3</sub> accounts for one-half or less of the total barium present after calcination and exposure to air [7,10]. Experimentally the presence of CO<sub>2</sub> does not prevent storage on BaO/Al<sub>2</sub>O<sub>3</sub> at 400 °C [8] although it does reduce the capacity of Pt/BaO/Al<sub>2</sub>O<sub>3</sub> [10,11] and also enhances release of  $NO_x$  [12].

The present work had two aims. One was to determine the extent to which water might also affect  $NO_x$  storage and release processes on alumina and baria/alumina. The other was to establish if reductants, CO and  $H_2$ , influenced the desorption characteristics. In practical Pt-containing catalysts, reduction of released gaseous  $NO_x$  would be expected to be small on the oxides compared to that on the metal(s). Nonetheless it is still of interest to know if decomposition of the stored material is itself influenced by the presence of reductants and this can be followed only if the metal is absent.

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### 2. Experimental

The experimental procedures used here were similar to those described in detail previously [8]. In essence, BaO/Al<sub>2</sub>O<sub>3</sub> containing 9 wt% Ba was made by successive impregnation of a washcoat-type alumina (Condea,  $140\,\mathrm{m}^2/\mathrm{g}$ ) using a solution of barium nitrate. After drying at  $110\,^\circ\mathrm{C}$ , it was calcined in flowing air for 3 h at  $\sim 500\,^\circ\mathrm{C}$ . Crystalline orthorhombic BaCO<sub>3</sub> (witherite) was then detectable by XRD but other studies on similar preparations indicate that this is likely to account for one-half or less of the total barium present [7,10]. The uptake and release of  $\mathrm{NO}_x$  was studied in a flow system using 40 mg samples contained in 4 mm i.d. quartz tubes and conditioned in flowing  $\mathrm{NO}_2/\mathrm{O}_2/\mathrm{He}$  on a ramp to 550 °C followed by He at 550 °C.

Uptake and release was measured from a stream containing ~1000 ppm NO<sub>2</sub>, 3% O<sub>2</sub> in a carrier of 0.07% Ar in He with a combined flow rate of 50 cm<sup>3</sup>/ min. The exit stream was analyzed by a quadrupole mass spectrometer (Balzers Thermostar), a micro gas chromatograph (MTI model M200) and, after dilution with a known flow of  $N_2$ , by a chemiluminescent  $NO_x$ analyzer (Ecotech model 9841) that determined NO and  $NO_x$  (NO + NO<sub>2</sub>) alternately on a  $\sim 12$  s cycle time. The mass spectrometer signals at m/z of 30 and 46 were processed to provide NO and NO<sub>2</sub> using a procedure that allowed for fragmentation and changes in sensitivity (when switching from streams without NO<sub>2</sub> to those with NO<sub>2</sub>) and then normalized against the chemiluminescent values. Similarly the mass spectrometer signals calculated for CO (from m/z = 28), O<sub>2</sub> (32),  $CO_2$  (44),  $H_2$  (2) and  $N_2$  (28 with  $H_2$  present, 14 with COpresent) were normalized to analyses by the chromatograph which has a sensitivity in the low ppm range for all except H<sub>2</sub>. The chromatograph enabled analysis for trace amounts of nitrous oxide. The system had a detection limit of ~10 ppm for ammonia using mass spectrometry (at m/z = 16) and, in one specific test, by on-line FTIR (with a resolution of 0.25 cm<sup>-1</sup>).

Blank tests using an empty reactor showed a small uptake and release of  $NO_2$  on metal components in the system that was somewhat greater with water present. The release plots that follow have been corrected for these effects.

### 3. Results and discussion

## 3.1. NO<sub>2</sub> uptake in the presence and absence of water

The present uptake measurement experiments were carried out at a lower temperature (300 °C) than the 400 °C used earlier [8] in order to minimize  $NO_x$  desorption prior to commencement of the temperature ramp during subsequent decomposition experiments. Data for uptake from  $\sim 1000$  ppm  $NO_2$  in 3%  $O_2/He$  in

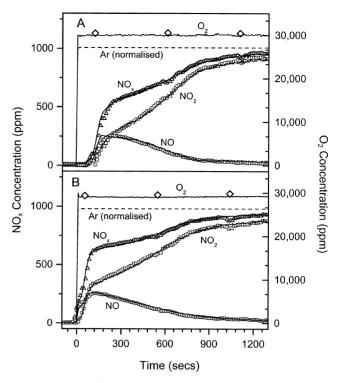


Figure 1. Uptake of NO<sub>2</sub> from  $\sim$ 1000 ppm NO<sub>2</sub> plus 3% O<sub>2</sub> in Ar/He on 40 mg BaO/Al<sub>2</sub>O<sub>3</sub> at 300 °C in the absence of water (A) and in the presence of  $\sim$ 1% water (B). Chemiluminescent analyzer and gas chromatograph, open symbols; mass spectrometer, solid line with Ar (dashed line) normalized to match NO<sub>2</sub> concentration after 3600 s.

the absence and presence of water are shown in figures 1(A) and (B) respectively. In the dry system there is an initial period lasting  $\sim\!80\,\mathrm{s}$  in which all  $NO_2$  is taken up, probably as surface nitrites if infrared measurements are a guide [4,5]. Thereafter uptake is partial and accompanied by the evolution of NO which exhibits a maximum concentration of  $\sim\!260\,\mathrm{ppm}$  after  $\sim\!210\,\mathrm{s}$ . The stoichiometry from then on corresponds approximately to reaction (1).

The presence of  $\sim 1\%$  ( $\sim 10\,000$  ppm) water eliminates the initial complete uptake entirely (figure 1(B)). Partial uptake with NO evolution is brought forward and then proceeds as with the dry stream. This is in accord with that expected for the reaction

$$Ba(OH)_2(s) + 3NO_2(g) \longrightarrow$$

$$Ba(NO_3)_2(s) + NO(g) + H_2O(g)$$
 (2)

Calculations carried out as described previously for the corresponding reaction involving BaCO<sub>3</sub> [8] indicated that the residual NO<sub>2</sub> concentration expected at equilibrium would be <1 ppm at 300 °C and that the potential extent of reaction would remain >97% until 520 °C.

NO<sub>2</sub> was also taken up on alumina alone at 300 °C but in smaller amounts. In the dry state the period of complete uptake was much shorter (<25 s) and, as found previously [8], the concentration of NO formed during the subsequent partial uptake was also less. The presence of water eliminated the period of complete

uptake entirely. Production of NO then reached a maximum almost immediately but there was little effect on the subsequent partial uptake.

# 3.2. Decomposition of stored $NO_x$ in the presence and absence of water

Water had no effect on the temperature-programmed decomposition of  $NO_x$  stored on alumina alone. In both situations, decomposition took place with concurrent peaks of  $NO_2$  and  $O_2$  at 430 °C. The  $NO_2/O_2$  ratio was  $\sim$ 4, as expected for the stoichiometric decomposition of a metal nitrate, with the maximum concentration of NO one-tenth that of  $NO_2$ .

Results for the decomposition of  $NO_x$  stored on  $BaO/Al_2O_3$  on a ramp at 5 °C/min in the presence and absence of water are shown in figure 2. The dry system (figure 2(A)) shows incompletely resolved peaks of first  $NO_2$  and then NO with maximum concentrations at 435 and 520 °C respectively. Although the peak concentration of NO is less than that of  $NO_2$ , it is accompanied by more  $O_2$  as expected if the decomposition is given by

$$Ba(NO_3)_2 \longrightarrow BaO + 2NO + 1\frac{1}{2}O_2$$
 (3)

rather than by

$$Ba(NO_3)_2 \longrightarrow BaO + 2NO_2 + \frac{1}{2}O_2$$
 (4)

With water present (figure 2(B)), decomposition proceeds distinctly differently. Evolution of  $NO_2$  is delayed with an initial peak reached at 455 °C and a second smaller one at 525 °C. The peak in NO concentration also occurs at a slightly higher temperature and is more sharply defined than for the dry system. Correspondingly, evolution of  $O_2$  proceeds more slowly to begin with than in the wet system with a subsequent well-defined maximum matching that of NO.

Overall it is apparent that water slows decomposition of  $NO_x$  stored on the barium-containing system. This is unexpected since on mass action grounds one would expect it to aid  $NO_x$  liberation via the reaction

$$Ba(NO_3)_2 + H_2O \longrightarrow Ba(OH)_2 + 2NO_2 + \frac{1}{2}O_2$$
 (5)

There are two potential explanations. One is that adsorbed water, or hydroxyl groups derived from it, interacts with the stored  $NO_x$  in some way and increases the binding energy. This has been reported at temperatures below 300 °C but not at higher temperatures [10], and seems unlikely especially as water has little effect on desorption from alumina. The alternative is that the  $NO_x$  initially released from the surface is replaced by a crust of  $Ba(OH)_2$  which impedes migration of the remaining  $NO_x$  lying underneath. The eventual onset of  $NO_x$  evolution cannot be associated with decomposition of bulk hydroxide, which has a calculated decomposition temperature of  $\sim$ 620 °C for the water pressure used here. However, it might reflect decomposition of a surface hydroxide that is less stable than the bulk form

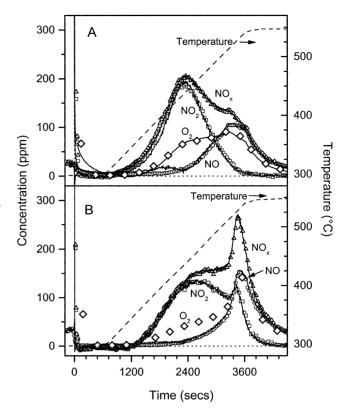


Figure 2. Decomposition of  $NO_x$  stored on 40 mg of  $BaO/Al_2O_3$  on a ramp to 550 °C at 5 °C/min: (A) into He alone after uptake as per figure 1(A); (B) into  $\sim$ 1%  $H_2O/He$  after uptake as per figure 1(B). Chemiluminescent analyzer and gas chromatograph, open symbols; mass spectrometer, solid lines with Ar dashed.

in the same way that dispersed carbonate appears less stable than bulk BaCO<sub>3</sub> [7]. It is also noteworthy that Ba(OH)<sub>2</sub> melts at 410 °C in which case transport of underlying NO<sub>x</sub> to the surface may become easier at higher temperatures.

# 3.3. Decomposition of stored $NO_x$ in the presence of CO and $H_2$

Decomposition of stored  $NO_x$  in the presence of reductants was carried out under dry conditions. The behavior with 5000 ppm CO present, shown in figure 3, is distinctly different from that in He (figure 2(A)).  $NO_2$  is observed in low concentrations only and confined to a narrow range of temperatures, 380–400 °C. In compensation, the peak concentration of NO is much higher and reached at a much lower temperature, 410 °C compared to 520 °C using helium alone. It is clear that CO is reducing  $NO_2$  according to

$$NO_2 + CO \longrightarrow NO + CO_2$$
 (6)

with some reaction at temperatures as low as 300 °C. It is also apparent from figure 3 that the fall-off in NO concentration above the maximum is associated with the production of  $N_2$  by further reduction

$$NO + CO \longrightarrow \frac{1}{2}N_2 + CO_2 \tag{7}$$

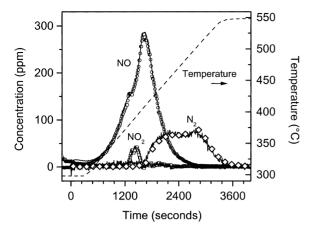


Figure 3. Decomposition of  $NO_x$  stored on 40 mg of  $BaO/Al_2O_3$  at 300 °C as per figure 1(A) into a stream of 5000 ppm CO in He on a ramp to 550 °C at 5 °C/min after 5 min of flushing in He. Chemiluminescent analyzer and gas chromatograph, open symbols; mass spectrometer, solid lines.

Very little ( $<5\,\text{ppm}$ )  $N_2O$  was formed and no  $O_2$  was detectable.

The corresponding result for the decomposition of stored  $NO_x$  in  $H_2$  is shown in figure 4, the pattern being intermediate between that observed with the other systems. The concentration of  $NO_2$  is higher than when using CO (figure 3) but less than in helium (figure 2(A)). Thus reduction of  $NO_2$  to NO by  $H_2$ 

$$NO_2 + H_2 \longrightarrow NO + H_2O$$
 (8)

is slower that the corresponding reduction by CO, reaction (6). Similarly, it is apparent that the further reduction of NO to  $N_2$  by  $H_2$ 

$$NO + H_2 \longrightarrow \frac{1}{2}N_2 + H_2O \tag{9}$$

is also slower than that by CO, reaction (7), since the fall-off in NO concentration associated with the onset of  $N_2$  production occurs at a higher temperature. Mole balance calculations indicated that hydrogen consumption was significantly greater than that which could be accounted for by reduction of  $NO_2$  to NO and  $N_2$ , suggesting that some ammonia might also be forming. However, none could be detected in the product stream by mass spectrometry or FTIR to the detection limit of  $\sim \! 10\,\mathrm{ppm}$ .

It may be noted that the  $NO_2$  concentrations registered by the chemiluminescent analyzer (open squares in figure 4) deviate from the mass spectrometer trace (continuous line) and become negative at temperatures above 450 °C. This behavior is the result of an instrumental artifact arising because some NO undergoes reduction by  $H_2$  within the chemiluminescent analyzer prior to the determination of total  $NO_x$  (i.e.  $NO+NO_2$ ). Ammonia, if present, might contribute to production of the same artifact but none was observed by mass spectrometry or FTIR as noted above.

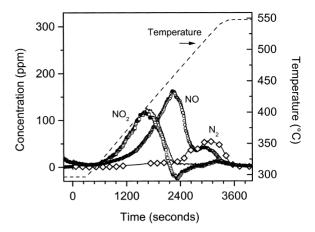


Figure 4. Decomposition of  $NO_x$  stored on 40 mg of  $BaO/Al_2O_3$  at 300 °C as per figure 1(A) into a stream of 2500 ppm  $H_2$  in He on a ramp to 550 °C at 5 °C/min after 5 min of flushing in He. Chemiluminescent analyzer and gas chromatograph, open symbols; mass spectrometer, solid lines.

If the decompositions of stored  $NO_x$  in He, CO and  $H_2$  are compared in terms of the total N being evolved, then it is apparent that the two reductants do facilitate the liberation process with maximum rates at 435, 414 and 429 °C respectively. The operative mechanism is probably through a reduction in the rate of readsorption, which is usually substantial during desorption from packed beds of porous particles [13,14]. With helium alone as the carrier, evolved  $NO_2$  molecules are likely to strike sites being vacated by other  $NO_2$  molecules during transport out of the system and hence be readsorbed. If they are reduced to NO and  $N_2$  then readsorption in the same form cannot occur and transport out of the system is facilitated.

Table 1 summarizes the quantities of  $NO_x$  stored in the experiments illustrated in figures 1–4 based on uptake and release measurements. The latter are likely to be more accurate since the slow approach to the plateau during uptake makes it difficult to determine when this process is complete. (The present calculations use the  $NO_x$  concentration after  $\sim$ 1 h as the cut-off point.) As may be seen, alumina appears responsible

Table~1 Uptake and release of  $NO_2$  for  $BaO/Al_2O_3$  and  $Al_2O_3$  at  $300\,^{\circ}C$ 

Substrate	H <sub>2</sub> O (%)	Reductant	Uptake (mmol/g) a	Release (mmol/g)
Al <sub>2</sub> O <sub>3</sub>	0	_	0.22	0.18 <sup>b</sup>
$Al_2O_3$	$\sim 1$	_	0.17	0.09 <sup>b</sup>
BaO/Al <sub>2</sub> O <sub>3</sub>	0	_	0.35	0.34 <sup>b</sup>
BaO/Al <sub>2</sub> O <sub>3</sub>	$\sim 1$	_	0.25	0.33 <sup>b</sup>
BaO/Al <sub>2</sub> O <sub>3</sub>	0	CO	0.33	0.43 <sup>c</sup>
BaO/Al <sub>2</sub> O <sub>3</sub>	0	$H_2$	0.37	$0.38^{d}$

<sup>&</sup>lt;sup>a</sup> At 300 °C from  $\sim$ 1000 ppm NO<sub>2</sub> in 3% O<sub>2</sub>.

 $<sup>^{\</sup>rm b}$  In He alone on temperature ramp from 300 to 550  $^{\rm o}{\rm C}$  at 5  $^{\rm o}{\rm C/min}.$ 

<sup>&</sup>lt;sup>c</sup> Calculated from sum of NO<sub>2</sub>, NO and N<sub>2</sub> produced (as shown in figure 3).

<sup>&</sup>lt;sup>d</sup> Calculated from sum of NO<sub>2</sub>, NO and N<sub>2</sub> produced (as shown in figure 4).

for approximately one-half the amount stored on BaO/Al<sub>2</sub>O<sub>3</sub> in the dry state while water reduces the uptake by up to 50%. Since the amount of barium in the sample is 0.59 mmol/g, the proportion converted to Ba(NO<sub>3</sub>)<sub>2</sub> in the dry state ( $\sim$ 0.18 mmol(NO<sub>x</sub>)/g) is 15% of the potential capacity. This is somewhat less than reported for Pt/BaO/Al<sub>2</sub>O<sub>3</sub> (e.g. 0.58 mmol(NO<sub>x</sub>)/g for a sample with 16.5 wt% Ba which corresponds to 24% of the potential capacity [10]).

### 4. Conclusions

Water reduces storage of  $NO_2$  on  $BaO/Al_2O_3$ , largely by eliminating the initial uptake that has been attributed to nitrite formation with little effect on the subsequent partial uptake that is accompanied by NO evolution and nitrate formation. Water has little effect on the temperature-programmed decomposition of any  $NO_x$  stored on alumina which takes place with evolution of  $NO_2$  and  $O_2$  and minimal NO. However, it does impede the decomposition of the more stable  $NO_x$  stored on barium which liberates NO as well as  $NO_2$ . Carbon monoxide and hydrogen enhance decomposition of stored  $NO_2$  under dry conditions by reducing  $NO_2$  to NO and  $N_2$ , with hydrogen being a less effective reductant than CO.

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